WHAT IS CLAIMED IS:

1. A method for upgrading a naphtha feed to a naphtha product containing less than about 10 wppm of nitrogen and less than about 15 wppm sulfur, the method comprising contacting said naphtha feed with hydrogen in the presence of a bulk multimetallic catalyst under effective reactor conditions to hydrodesulfurize and hydrodenitrogenize said naphtha feed to produce said naphtha product, wherein said bulk multimetallic catalyst comprises at least one Group VIII non-noble metal and at least two Group VIB metals.

2. The method of claim 1, wherein said bulk multimetallic catalyst is made by reacting insoluble or partially insoluble metal salts of said metals in the presence of a protic liquid.

3. The method of claim 1, wherein said bulk multimetallic catalyst is made by combining and reacting at least one Group VIII non-noble metal component with at least two Group VIB metal components in the presence of a protic liquid, with at least one of the metal components remaining at least partly in the solid state during the entire catalyst making, said Group VIII and Group VIB metals comprising from about 50 wt.% to about 100 wt.%, calculated as oxides, of the total weight of said bulk catalyst particles, with the solubility of those of the metal components which are at least partly in the solid state during the reaction being less than 0.05 mol/100 ml water at 18°C.

4. The method of claim 1, wherein the bulk multimetallic catalyst is made by combining and/or reacting dissolved metal salts in a protic liquid to form a precipitate.

5. The method of claim 1, wherein said bulk multimetallic catalyst has been subjected to a sulfidation treatment.

6. The method of claim 1, wherein the Group VIII non-noble metal is selected from the group comprising cobalt, nickel, iron, or mixtures thereof, and the Group VIB metals are selected from the group comprising chromium, molybdenum, tungsten or mixtures thereof.

7. The method of claim 1, wherein the Group VIII non-noble metal consists substantially of nickel and the Group VIB metals consist substantially of molybdenum and tungsten.

8. The process of any one of the preceding claims, wherein the bulk catalyst particles are subjected to one or more of the following process steps:

(i) compositing with a material selected form the group of binder materials, conventional hydroprocessing catalysts, cracking components, or mixtures thereof,

(ii) spray-drying, (flash) drying, milling, kneading, slurry-mixing, dry or wet mixing, or combinations thereof,

(iii) shaping,

(iv) drying and/or thermally treating, and

(v) sulfiding.

9. The method of claim 1, wherein said naphtha feed is selected from the group consisting light and full range virgin naphthas, catalytically cracked naphthas, delayed coking naphtha, fluid coking naphtha, and contact coking naphtha.

10. The method of claim 1, wherein said naphtha feed is a heavy catalytically cracked naphtha having a boiling range of from about 250°F to about 420°F, and comprises aromatics, olefins, sulfur compounds, and nitrogen compounds.

11. The method of claim 1, further comprising a flashing or fractionation step following said hydrotreating step to release any gaseous byproducts and collect the desulfurized and denitrogenized naphtha.

12. The method of claim 1, wherein said effective reactor conditions include a temperature from about 100°C to about 370°C, a pressure from about 10 to about 60 bar, a hydrogen to naphtha ratio from about 100 to about 2,000 standard cubic feet of hydrogen per barrel of feed, and a space velocity from about 0.5 to about 15 LHSV.

13. A method for upgrading a naphtha feed to a naphtha product containing less than about 10 wppm of nitrogen and less than about 15 wppm sulfur, the method comprising reacting said naphtha in at least one reaction stage, in the presence of a hydrogen containing gas, as it passes through two or more catalyst beds, wherein at least one catalyst bed comprises a multimetallic catalyst comprising at least one group non-noble metal and at least two Group VIB metals, wherein the ratio of Group VIB metals to Group VIII non-noble metals is about 10:1 to about 1:10, and wherein said at least one reaction stage is

operated at an effective temperature and hydrogen pressure to hydrodesulfurize and hydrodenitrogenize the naphtha feed to produce said naphtha product.

14. The method of claim 1 or 12, wherein said naphtha feed is naphtha from a fluid catalytic cracking unit having a specific gravity from about 0.7 to about 0.9, API from about 33 to about 41, sulfur content from about 0.2 to about 0.5 percent by weight, nitrogen content from about 50 to about 100 wppm, aromatics from about 50 to about 90 percent by weight, and olefins from about 2 to about 9 percent by weight.

15. The method of claim 1 or 13, wherein said naphtha feed is naphtha from a fluid catalytic cracking unit having a specific gravity from about 0.8 to about 0.87, API from about 35 to about 39, sulfur content from about 0.3 to about 0.4 percent by weight, nitrogen from about 65 to about 85 wppm, aromatics from about 60 to about 80 percent by weight, and olefins from about 4 to about 7 percent by weight.

16. A two stage method for reducing the sulfur content of a naphtha feed comprising:

(a) reacting said naphtha feed in a first stage in the presence of a hydrogen-containing treat gas, said first stage containing one or more reaction zones operated under effective conditions and in the presence of at least one first stage HDS catalyst for producing a first liquid product stream having a substantially reduced sulfur content;

(b) passing said first product stream to a separation zone to form a vapor phase product stream and a second liquid product stream;

(c) reacting said second liquid product stream in a second stage in the presence of a hydrogen-containing treat gas, said second stage containing one or more reaction zones operated under effective conditions and in the presence of at least one second catalyst for producing a naphtha product stream having less than about 15 wppm sulfur; and

(d) recovering said naphtha product stream.

17. The method of claim 15, wherein said naphtha product stream has less than about 10 wppm sulfur.

18. The method of claim 15, wherein said naphtha product stream has less than about 5 wppm sulfur.

19. The method of claim 15, wherein said at last one first or second stage catalyst is a bulk multimetallic catalyst comprising at least one group non-noble metal and at least two Group VIB metals, wherein the ratio of Group VIB metals to Group VIII non-noble metals is about 10:1 to about 1:10, and wherein said at least one reaction stage is operated at an effective temperature and hydrogen pressure to hydrodesulfurize and hydrodenitrogenize the naphtha feed to produce said naphtha product.

20. The method of claim 15 further comprising a third hydroprocessing stage.

21. The method of claim 15, wherein said bulk multimetallic catalyst is made by reacting insoluble or partially insoluble metal salts of said metals in the presence of a protic liquid.

22. The method of claim 15, wherein said bulk multimetallic catalyst is made by combining and reacting at least one Group VIII non-noble metal component with at least two Group VIB metal components in the presence of a protic liquid, with at least one of the metal components remaining at least partly in the solid state during the entire catalyst making, said Group VIII and Group VIB metals comprising from about 50 wt.% to about 100 wt.%, calculated as oxides, of the total weight of said bulk catalyst particles, with the solubility of those of the metal components which are at least partly in the solid state during the reaction being less than 0.05 mol/100 ml water at 18°C.

23. The method of claim 15, wherein said bulk multimetallic catalyst has been subjected to a sulfidation treatment and wherein the Group VIII non-noble metal is selected from the group comprising cobalt, nickel, iron, or mixtures thereof, and the Group VIB metals are selected from the group comprising chromium, molybdenum, tungsten or mixtures thereof.